La biolixiviation: apport des biotechnologies pour la valorisation du contenu métallique des déchets

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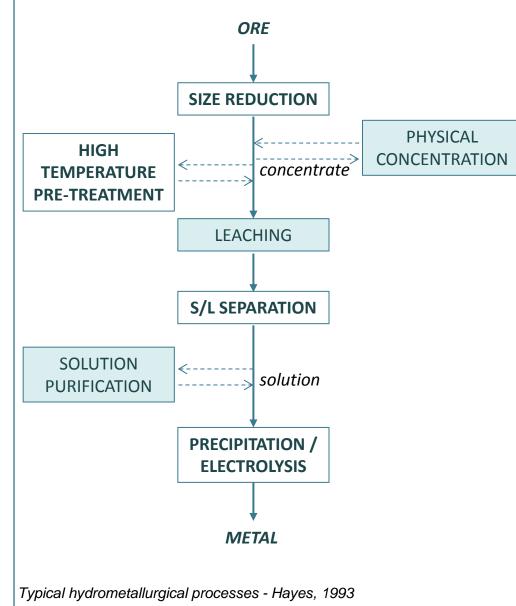
 What is Bioleaching? At the interface between Micro-Organisms (biology) and Minerals (geology)...

Current status and case study (reprocessing of mine wastes)

Some challenges and perspectives



What is « Bio-Hydrometallurgy »?



Hydrometallurgical reactions assisted with microbial activities:

- Bio-flotation: modification of mineral surfaces to enhance or depress flotation
- Bio oxidation: microbial catalyzed oxidation (especially of Fe²⁺ and S species)
- Bio-complexation: generation of organic compounds that favorably complex with metal species
- Bio-sorption/ -accumulation: incorporation of metal species from solution into biomass

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What is « Bioleaching »?

Microbially assisted leaching of certain minerals (Biooxidation/Bio-complexation):

 Bioleaching can be applied to various ore types through microbial generation of leach agents:

Se.g.1: H⁺ and Fe³⁺ leaching mineral sulfides -> *Bio-oxidation*e.g.2: organic acids leaching oxides and laterites -> *Bio-complexation*e.g.3: biogenic cyanide for gold leaching -> *Bio-complexation*

Organic acid and cyanide bio-production remains at laboratory stage:

slow rates and low yields of metal extraction as well as the cost of microbial substrates (glucose, etc.) and the production of excess biomass have precluded these approaches being developed as commercial operations

 Most R&D has focused on BIO-OXIDATION which is the only bioleaching process to reach industrial implementation.



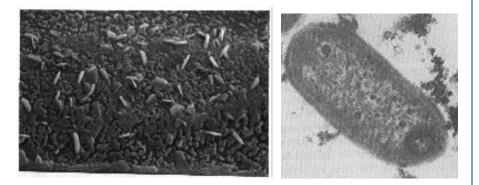
Bioleaching/Biooxidation

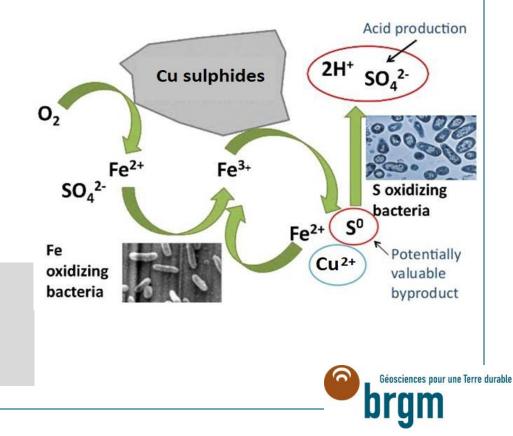
How does it work?

- Bacterial degradation of the sulfide matrix:
 - Solution of ferrous iron and sulfur = energy source
- Liberation and/or solubilisation of the metals in acidic media
 - H_2SO_4 = a product of the bacterial metabolism
- Acidophilic, autotrophic bacteria (heterotrophic), from 30°C to 80°C (mesophiles, moderate thermophiles, thermophiles)
 - Leptospirillum ferriphilum, Acidithiobacillus caldus, Sulfobacillus benefaciens, Sulfolobus sp...

∜ aerobic

 $\begin{array}{l} \text{MS}+2\text{Fe}^{3+}\rightarrow\text{M}^{2+}+2\text{Fe}^{2+}+\text{S}^{0}\\ 2\text{Fe}^{2+}+0.5\text{O}_{2}+2\text{H}^{+}\rightarrow2\text{Fe}^{3+}+\text{H}_{2}\text{O} \ (bact.)\\ \text{S}^{0}+1.5\text{O}_{2}+\text{H}_{2}\text{O}\rightarrow2\text{H}^{+}+\text{SO}_{4}^{2^{-}} \ (bact.) \end{array}$





Bioleaching/Biooxidation

Solubilisation of metals (associated to sulfide matrix) by bacteria, a natural phenomenon known and used since earliest Antiquity:

- Acid mine drainage
- Metals recovery, especially Cu
- \rightarrow Rio Tinto: Cu exploitation from Phoenician times; 1st heap bioleaching attested in the 17th century



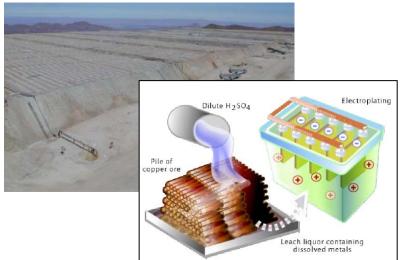




Bioleaching/Biooxidation

Bio-hydrometallurgy = an established technology and an industrial reality for ore processing

Heap leaching



Current status

- Mainly applied for the treatment of Cu Ores
- Many bioheap processes have targeted extraction of marginal ores not suitable for concentration and smelting
- Main operators : Newmont Mining, BHP Billiton, RioTinto, Codelco,...

Stirred tank reactor



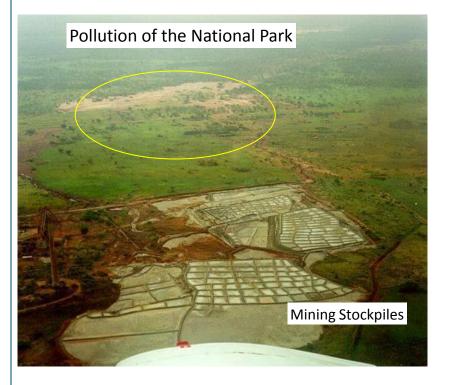
Current status

- Mainly applied to refractory gold (Biox process) and some base metals (Co, Ni, Cu...)
- More than 15 plants in operation at industrial or demonstration scale
- Main operators : Newmont Mining, BHP Billiton, RioTinto, Codelco,...



Bioleaching application for mine tailings reprocessing and metal recovery

KCC (Kasese Cobalt Company): An industrial project of cobalt recovery using bioleaching technology as an answer to an environmental issue



Context: Kilembe Mine - Kasese (Uganda)

- Former Cu mine -> 1,1 million tons of tailings
- Fine (<200µm) and heavy material (d ± 4.5)
- Pyrite FeS2: 80%
- 1.38% cobalt disseminated in the pyrite lattice

Biology:

- Identification of a biological activity around the stockpiles and in the drainage: natural bioleaching process
- Mesophile to moderate thermophile microbial consortium (Leptospirillum ferriphilum, Acidithiobacillus caldus, Sulfobacillus benefaciens...)
- Preliminary bioleach amenability tests in lab: more than 95% of Co recovery

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- A way to stop the discharge trail from the KASESE site to the Queen Elisabeth National Park due to runoff and natural bioleaching of the concentrate
- ✤ An alternative to technologies which are air-polluting (roasting), or energy consuming (roasting and high-pressure leaching)

KCC project: a bioleach success story

- 1989-91: Pre-feasibility study
 - testwork on bioleaching at lab-scale (2L stirred tank reactor, batch)
 - -> main operating parameters (temperature, pH) and microbial monitoring)
- 1992-1993: Feasibility step I
 - bioleaching pilot testwork in BRGM process hall (100L STR, 5 kg/d)

-> residence time, solid load, mass transfer (pulp homogeneity, gas dispersion), energy transfer (thermal regulation), pH regulation...

- 1993-96: Feasibility step II and basic engineering
 - Complementary testwork on bioleaching, zinc solvent extraction and electrowinning
 - Bioleaching pilot testwork: 1t per day in Uganda 65 m3 tank
 - Environmental impact study & Power supply (hydroelectric)
 - Engineering and economic evaluation, feasibility report and auditing
- 1996-98: Detailed engineering
- 1998-99: Construction and start-up -> first Co cathode in June 1999
- 2002: Monthly cobalt production reaches 67 tons (~ 2% of the world Co production)
- 2014: End of the operation All the tailings stockpiles have been treated and the site environment has been restored!!!













Some challenges and perspectives

The improvement of process efficiency (and economy):

Improvement of gas transfer:

- 2 kg of oxygen is needed to convert 1 kg of sulfide (for ex., the dissolution of 1 kg of pyrite requires 1 kg of oxygen)
- Solution The oxygen uptake rate (OUR) depends on the kinetics of the chemical and biological reactions and can vary with the type of micro-organisms. In optimal conditions, <u>OUR varies between 800 and 2000</u> <u>mg/L/h.</u>
- ⇔ Main CAPEX: Agitator. Main OPEX: Energy to inject and to disperse the gas (air and CO2)
- Scientific challenges: impellers design, replacement of air by oxygen (microbial tolerance to increasing dissolved oxygen concentration)

Increase of solid load:

- ♦ The solid load in the feeding pulp is comprised between 10% and 20%, and usually around 15%.
- Some of the main CAPEX for bioleaching processes is the cost of the tanks. Increasing solid load means decreasing the size and the number of tanks and thus their cost.
- & Scientific challenges: oxygen transfer, metal tolerance, microbial resistance to shear stress

Reactor design:

In between heap and STR

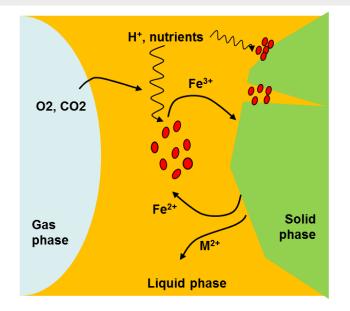
The adaptation of the technology to new types of metals bearing targets:

- Primary base metals resources (mainly Cu...) -> Process economy
- Oxyde ores (laterites) -> reprocessing of untreated limonitic stockpiles (Ni, Co, Cu + REE, Sc...)





Improvement of gas transfer



$$\begin{split} MS + 2Fe^{3+} &\xrightarrow{chemical} M^{2+} + 2Fe^{2+} + S^0 \\ 2Fe^{2+} + \frac{1}{2}O_2 + 2H^+ &\xrightarrow{bact.} 2Fe^{3+} + H_2O \\ S_0 + &\frac{3}{2}O_2 + H_2O &\xrightarrow{bact.} 2H^+ + SO_4^{2-} \end{split}$$

42°C								
Partial pressure	O ₂ Solubility C* (mg/L)							
20%	6							
30%	9							
40%	12							
50%	15							
60%	18							
70%	21							

$$R_{O2} = OTR = k_L a \times (C^*_{O2,L} - C_{O2,L})$$
volumetric G/L transfer coefficient driving force

$C^* = (P_{O2}^*/H_{O2}) = (P_{O2}/H_{O2})$ Henry's law

How to improve O₂ transfer?

Increase transfer coefficient

♦ Mixing system

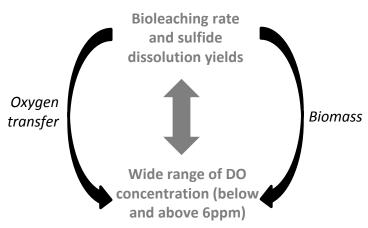
Increase the driving force

To replace air by O_2 enriched gas or pure O_2

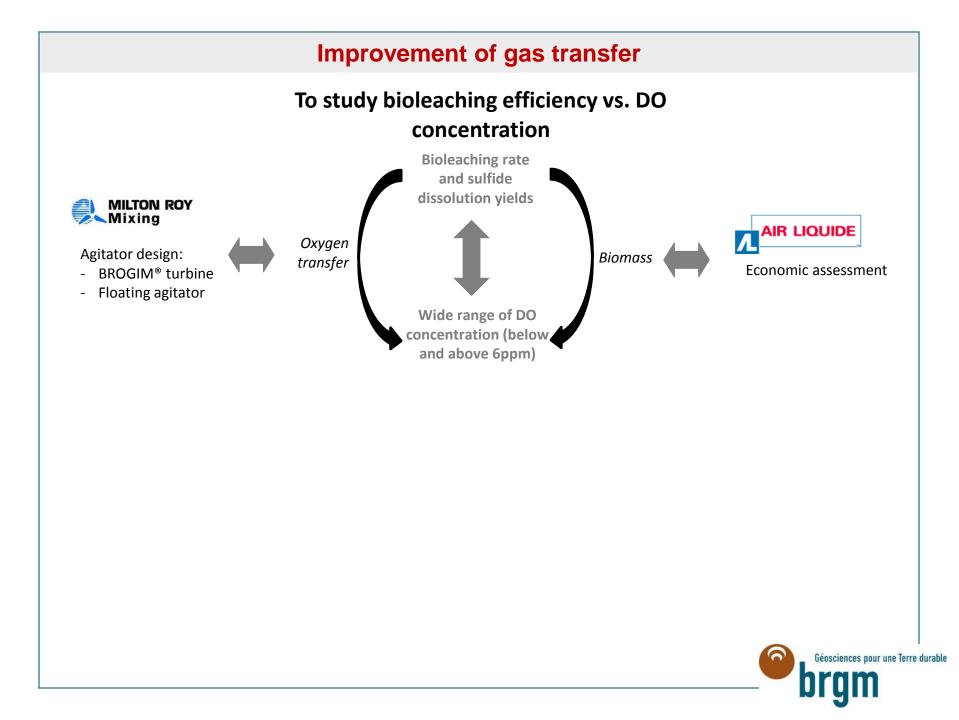
→ Main issue: the DO concentration will increase, which might affect bacterial activity. See the recent work of Wang et al. (2015) who observed a decrease of bacterial activity for DO > 5 mg/L

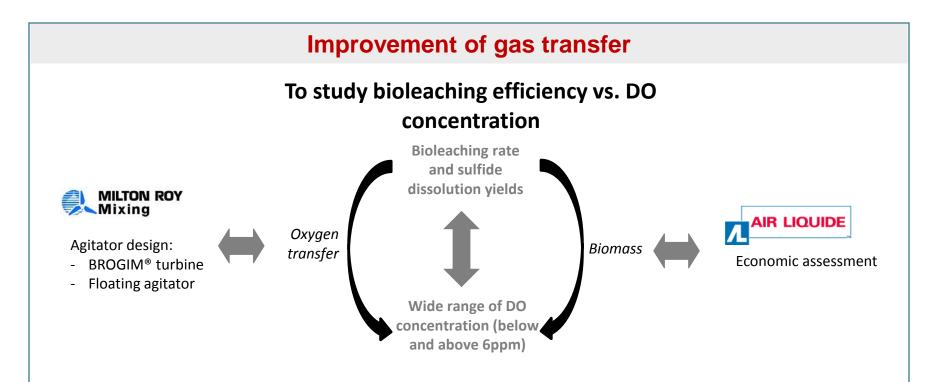


Improvement of gas transfer To study bioleaching efficiency vs. DO concentration









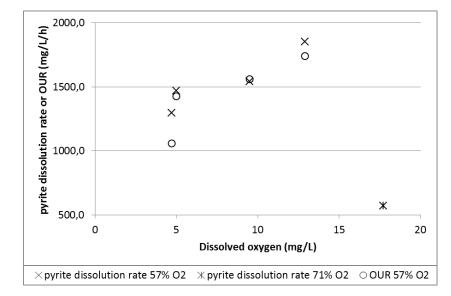
Experimental design: bioleaching in continuous mode (20L STR, 20% solid, , 5kg/d, 2 days residence time, 4 months of operation, 5kg/d)

- Time and HR consuming
- Numerous failures (pumps, plugging...)
- Few tested conditions
- Exhausts operators'patience

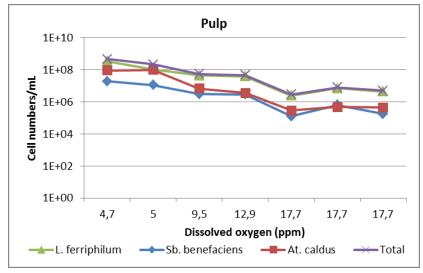
- Enables to operate at steady state -> avoids DO variation due to changes in O₂ demand
- Reliable analysis of the gas phase -> reliable OTR quantification

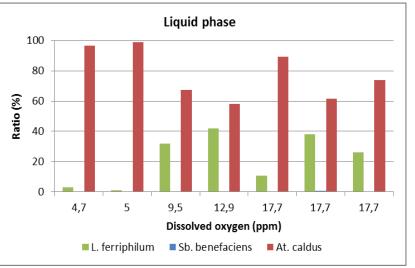


Improvement of gas transfer

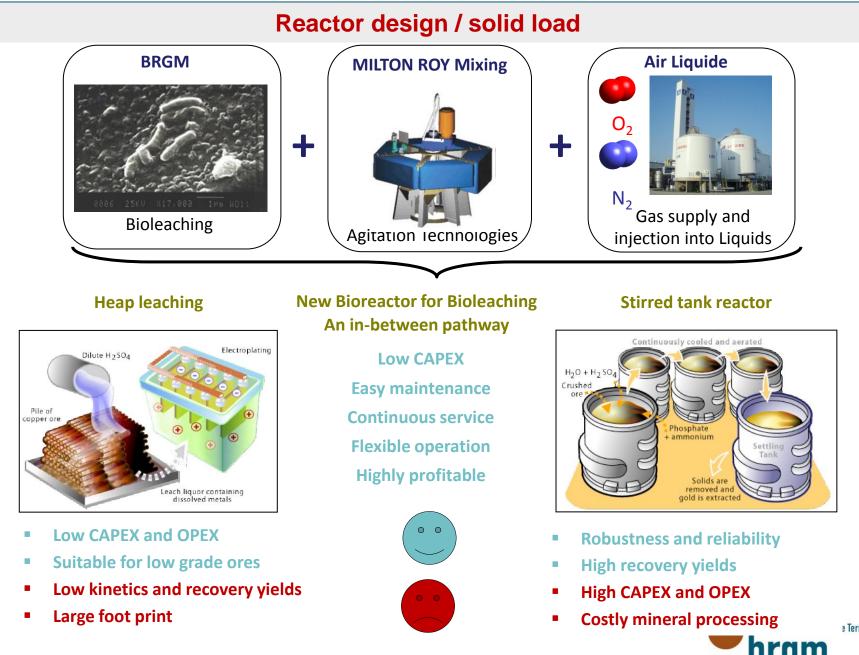


	measured DO concentration	Residence time	Sulfide dissolution yield		
	ррт	Day	%		
Condition 1	4,7	2,5	63%		
Condition 2	5,0	2,2	56%		
Condition 3	9,5	2,2	61%		
Condition 4	12,9	2,2	77%		
Condition 5	17,7	2,4	29%		



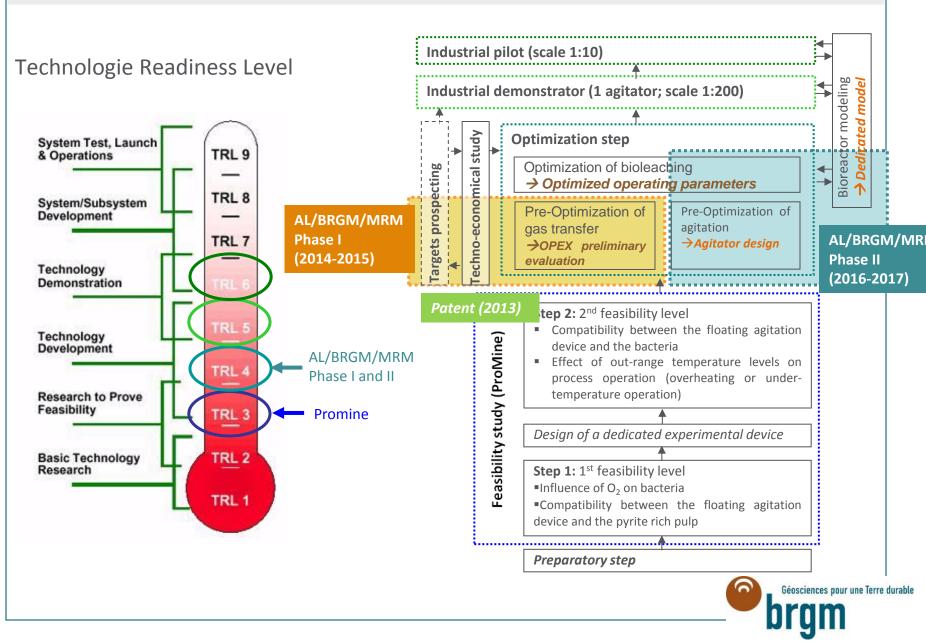






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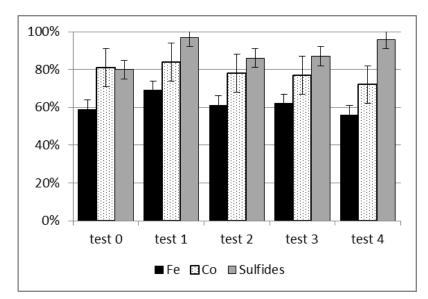
Reactor design / solid load



Reactor design / solid load

Experimental conditions	Test 0	Test 1	Test 2	Test 3	Test 4
Solid load	20%	20%	20%	20%	30%
O ₂ partial pressure	air	30%	50%	70%	70%
Maximum gas flow rate (m ³ /h)	6	2	1,2	0,9	0,9
Mean DO concentration (ppm)	2	4	8	14	14

	Test 0	Test 1	Test 2	Test 3	Test 4
Leaching rate (mgCo/L/d)	9 (± 1)	13 (± 1)	12 (± 1)	11 (± 1)	12 (± 1)



Batch tests in 1,5 m3 tank Tested parameters: solid load and gas composition (oxygen enrichment), bacterial tolerance towards agitation device, gas transfer

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Materials: sulfide rich tailings (60% pyrite, 600 ppm Co)

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Bioleaching and WEEE recycling?

Objective

Metal recovery in "atmospheric conditions" with lower environmental impacts

Targets

 Mainly focused on "Low-grade" Printed Circuit Board, but can be applied to any type of metal rich wastes

Current status

Lab-scale to piloting scale

Two types of bacteria

- Heterotrophic bacteria: production of biogenic acids for base metals solubilisation or production of cyanide for noble metals recovery

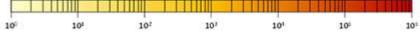
 - $\red S$ Consumption of cyanide by Cu
- Autotrophic bacteria: bacteria act as catalyzers that promote the recycling (re-oxidation) of FeII in FeIII and the production of H₂SO₄ (similar to bioleaching of sulfidic minerals) which are used to solubilize metals
 - ♥ PCBs toxicity (metal tolerance)
 - Chemicals consumption: PCBs are highly acid-consumming...
- → Autotrophic bacterial leaching remains the most promising way but requires further improvement...

Similar technology applied at industrial pilot scale for metal recovery for automotive shredded residues (Phoenix project, Comet, Belgium)



Bioleaching and WEEE recycling?

Η																	He
Li	Be	Ì.										В	с	N	0	F	Ne
Na	Mg											Al	Si	р	S	CI	Ar
к	Ca	Sc	Ti	۷	Cr	Mn	Fe	Со	Ni	Gu	Zn	Ga	Ge	As	Se	Br	Kr
Rb	Sr	Y	Zr	Nb	Мо	Тс	Ru	Rh	Pd	Ag	Cd	In	Sn	Sb	Te	1	Xe
Cs	Ba		Hf	Ta	w	Re	Os	lr	Pt	Au	Hg	TI	Pb	Bi	Ро	At	Rn
Fr	Ra		Rf	Db	Sg	Bh	Hs	Mt	Ds	Rg	Cn	Uut	FI	Uup	Lv	Uus	Uuc
• La	nthan	ides	La	Ce	Pr	Nd	Pm	Sm	Eu	Gd	Tb	Dy	Но	Er	Tm	Yb	Lu
	Actinic	des	Ac	Th	Pa	U	Np	Pu	Am	Cm	Bk	Cf	Es	Fm	Md	No	Lr



	Xiang et	Ilyas et	Ilyas et	Wang et	Zhu et al.
	al. (2010)	al. (2007)	al. (2013)	al. (2009)	(2011)
PCB content (g.L ⁻¹)	20	10	100	7.8	8
time (day)	16	18	12	5	3
% diss. Cu	95%	74%	90%	70%	92.9%



Bioleaching and WEEE recycling: BRGM recent work

Context:

- At least 5000 Km of Europe's rivers are contaminated with acid mine drainage (AMD) which is formed by microbiological weathering of sulfidic mine waste
- ⇔AMD = acidic, ferric iron-rich run off
- Segular major accidents caused by AMD
 (Aznacolar, Baia Mare...) → environmental and health impacts



Purpose:

to develop a novel bioleaching process based on a co-processing approach for the recovery of metals contained in waste PCBs using sulfidic mining wastes as a source of lixiviant

Objectives:

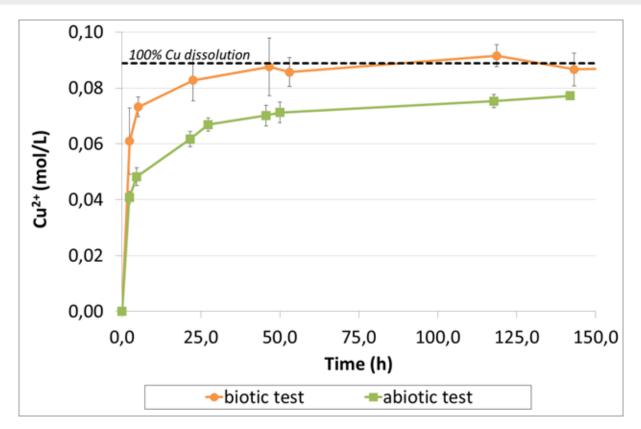
 Enhancing metal recovery in both wastes
 Decreasing environmental impacts linked to mining wastes (AMD)

Treatment principles (2-steps process):

- ⇔ Biological oxidation of the sulfidic wastes using acidophilic bacteria → production of a ferric iron-sulfuric acid leaching solution
- ♥PCBs leaching → solubilisation of base metals (Cu + Zn, Ni, Sn, Co, Ga...)



Bioleaching and WEEE recycling: BRGM recent work



Biotic tests:

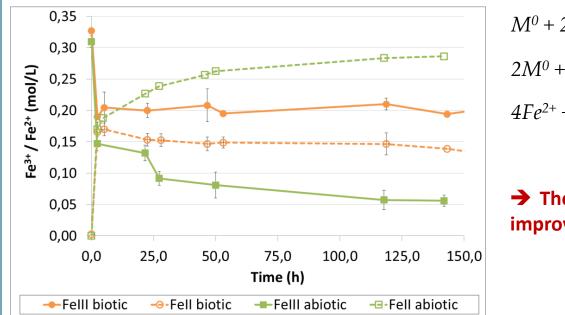
- 82% of Cu extraction after 5h
- 92% of Cu extraction after 24h
- No addition of H₂SO₄

Abiotic tests:

- 58% of Cu extraction after 5h
- 78% of Cu extraction after 24h
- Addition of H₂SO₄ to maintain the pH below 2
- → The use of biological leaching solution improves the leaching efficiency...



Bioleaching and WEEE recycling: BRGM recent work



$$\begin{split} M^{0} + 2Fe^{3+} &\longrightarrow M^{2+} + 2Fe^{2+} \text{ (fast)} \\ 2M^{0} + 4H^{+} + O_{2} &\longrightarrow 2M^{2+} + 2H_{2}O \text{ (slow)} \\ 4Fe^{2+} + O_{2} + 4H^{+} &\longrightarrow 4Fe^{3+} + 2H_{2}O \text{ (bact.)} \end{split}$$

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→ The bacterial recycling of FeIII improves leaching kinetics...

		One-step leaching								
	Xiang et al. (2010)	Ilyas et al. (2007)	Ilyas et al. (2013)	Wang et al. (2009)	Zhu et al. (2011)	This study				
PCB content (g.L ⁻¹)	20	10	100	7.8	8	25				
time (day)	16	18	12	5	3	1 2				
% diss. Cu	95%	74%	90%	70%	92.9%	93%	99%			

Some perspectives

Improvement of gas transfer:

- Modelling of oxygen transfer
 Assessment of DO micro-heterogeneity in the reactor
- Investigation of oxygen toxicity mechanisms

Reactor design:

- Pilot demonstration with a copper sulfidic ore -> technical and economic assessment of the technology
- Secometric (German and French ANR project)

Beyond BRGM work:

MUNDO bioleach plant (Finland): reprocessing of tailings produced by talc ore treatment for the recovery of Co and Ni

- Acquisition of BIOX process by OUTOTEC -> OKTOP[®] reactor plant for gold ore pre-treatment
- PHOENIX project launch in Belgium: bioleach process to recover metals in automotive shredded residues

WEEE recycling:

- PhD to investigate:
 - Leaching mechanisms
 - Microbial tolerance toward metals
- Chaire Paris Tech "Mines Urbaines" -EcoSystemes
- Demonstration of the co-processing concept (sulfidic wastes + PCBs) at pilot scale (Polish coal waste)
- ✤ CERES EU project (RFCS call)

